

Optimizing and accelerating history matching progress of numerical reservoir simulation by using material balance analysis

Yaozhong Yang^{1,*}, Jinbiao Yu², Yong Wang², and Chengjie Ma¹

¹Information management center of Shengli Oilfield Company Ltd., Sinopec, 257015, DongYing, ShanDong, China

²Research Institute of exploration and development of Shengli Oilfield Company Ltd, 257015, DongYing, ShanDong, China

Keywords: Material balance analysis, Numerical reservoir simulation, Optimization and acceleration, Uncertainty analysis.

Abstract. In view of the problem of huge computations and multiple solutions, a method for optimizing and accelerating the progress of history matching by using material balance analysis was established. Based on simple measuring data, such as average pressure, daily production rate and PVT test, a material balance model can be constructed for a three phase system of hydrocarbon reservoir. According to the material balance calculation, original oil in place and aquifer parameters can be obtained as optimized parameters for numerical simulation, which contributes to solve the multi-solutions problem of history matching. Besides, by conducting uncertainty analysis using Monte-Carlo simulation method, one can determine the adjustment range of input parameters, which helps the engineer definite a clear direction, reduce the number of computations and consequently accelerate the progress of history matching. The reliability of the proposed method was verified according to two examples.

1 Introduction

The advantage of reservoir numerical simulation is that it can integrate different types of data, such as geology, geophysics, reservoir fluid and rock properties, into one platform for production prediction. There is a great deal of uncertainty in reservoir model, which needs to be modified by history matching. History matching has a huge amount of computation and the results have multiple solutions, If a reasonable initial condition and adjustable range of parameters can be screened out before history matching, the uncertainty can be greatly reduced, the process of matching can be optimized and more reasonable combination of reservoir parameters can be obtained.

* Corresponding author: machengjie.slyt@sinopec.com

Before the rapid development and wide application of reservoir numerical simulation technology, material balance method was used in reservoir development management as an important tool for reservoir performance analysis. With the continuous development of computer technology, the material balance method based on zero dimensional model is gradually replaced by exquisite three-dimensional reservoir numerical simulation. This is mainly because the principle of material balance is applied to every grid scale in reservoir numerical simulation, and it seems that separate material balance analysis has become unnecessary. However, compared with numerical simulation, the material balance analysis method has the following advantages:

(1) There are many uncertainties in 3D reservoir model, which are related to reservoir shape, petrology, geophysics and so on. However, the material balance equation is only based on the conservation of production, pressure and PVT data, and its uncertainty is relatively small.

(2) It is impossible to obtain the contribution rate of different driving energy to production only by 3D reservoir model, and the influence degree of different model parameters on matching indexes can not be judged in advance. Parameter adjustment is often decided by experience and personal judgment. By calculating the driving index, the material balance analysis method can quantitatively give the different driving energy sources in the oil and gas production process.

(3) The material balance analysis method studies the relationship between the geological reserves, the remaining reserves and the recovery of the reservoir. It does not involve the flow direction of the fluid, and does not consider the spatial changes of rock and fluid properties, the hydrodynamic factors of fluid flow in porous media, fluid differentiation, reservoir geometry, well location or production of different fluids.

Through the above analysis, we think that before the numerical simulation, some valuable information can be obtained through the material balance analysis, which can be used to guide the reservoir numerical simulation. Therefore, this paper establishes an accelerated method of historical matching optimization of reservoir numerical simulation based on material balance analysis. Through the research of predicting global sensitivity parameters and uncertainty analysis, it forms the overall macro understanding of the reservoir and accelerates the process of historical matching.

2 Material balance equation

Since Schilthuis R J [1] first established the material balance equation of reservoir based on the principle of material conservation in 1936, it has been widely applied and developed in reservoir engineering. It is one of the basic methods for reservoir engineers to interpret and predict reservoir dynamics.

2.1 General equation of material balance

The linear form of the material balance equation is

$$F = NE_t + W_e \quad (1)$$

where :

$$F = N_p (B_o - B_g R_s) + (G_p - G_i) B_g + (W_p - W_i) B_w \quad (2)$$

$$E_t = E_o + mE_g + E_{fw} \quad (3)$$

$$E_o = (B_o - B_{oi}) + (R_{si} - R_s) B_g \tag{4}$$

$$E_g = B_{oi} \left(\frac{B_g}{B_{gi}} - 1 \right) \tag{5}$$

$$E_{fw} = (1+m) B_{oi} \cdot \frac{C_w S_{wc} + C_f}{1 - S_{wc}} (p_i - p) \tag{6}$$

where N is initial oil reserves, sm^3 ; m is gas cap ratio, $m = GB_g / NB_o$, G is gas reserves of gas cap, sm^3 ; N_p, W_p, G_p, W_i, G_i and W_e is cumulative oil production, cumulative water production, cumulative gas production, cumulative water injection, cumulative gas injection, cumulative water influx in turn, sm^3 ; p_i is initial reservoir pressure, MPa; p is average reservoir pressure, MPa; B_o is crude oil volume factor, rm^3/sm^3 ; R_s is dissolved gas oil ratio, sm^3/sm^3 ; B_g is gas volume factor, rm^3/sm^3 ; C_w is compressibility of formation water, MPa^{-1} ; C_f is rock compressibility, MPa^{-1} ; S_{wc} is irreducible water saturation.

In general, the production data can be obtained directly from the field, the average formation pressure can be measured by the downhole pressure gauge, and the pressure-volume-temperature parameters of fluids and rocks can be measured by the laboratory. The original oil in place N , gas cap ratio m and aquifer influx W_e is unknown. Among those variables, the aquifer influx W_e is the function of aquifer radius r_a , thickness h , permeability k_a , total compressibility c_t , Water influx Angle θ and so on. The aquifer influx is the very important part of material balance equation. There are various models and methods to calculate water influx [1-6]. For convenience, we use two common analytical aquifers of Eclipse in this paper. They are Carter-Tracy unsteady aquifer[5] and Fetkovich pseudo-steady aquifer [6].

2.2 Water influx calculate model

The linear form of the material balance equation

(1) Carter-Tracy unsteady aquifer

In 1960, Carter-Tracy put forward the approximate calculation formula of water influx based on the Hurst-van Everdingen aquifer model.

the cumulative water influx in t_n is :

$$(W_e)_n = (W_e)_{n-1} + [(t_D)_n - (t_D)_{n-1}] \times \left[\frac{B \Delta p_n - (W_e)_{n-1} (p'_D)_n}{(P_D)_n - (t_D)_{n-1} (P'_D)_n} \right] \tag{7}$$

where B is influx constant, rm^3/day ; t_D is dimensionless time; Δp_n is overall pressure drop in t_n , MPa; P_D is dimensionless pressure; P'_D is dimensionless derivative of pressure; which is calculated by the follow formula :

$$B = 2\pi\phi c_i r_e^2 h f \tag{8}$$

$$t_D = t_c t = 8.64 \times 10^{-2} \frac{k_a t}{\phi \mu_w c_i r_e^2} \tag{9}$$

(2) Fetkovich pseudo-steady aquifer

In 1971, Fetkovich put forward a new approximate calculation formula of water influx. the water influx formula in the n th time step is:

$$(\Delta W_e)_n = \frac{W_{ei}}{p_i} \left[(\bar{p}_a)_{n-1} - (\bar{p}_r)_n \right] \left[1 - \exp\left(-\frac{J p_i \Delta t_n}{W_{ei}}\right) \right] \tag{10}$$

So, the cumulative water influx in t_n is :

$$W_e = \sum_{i=1}^n (\Delta W_e)_i \tag{11}$$

In this formula, $(\bar{p}_a)_{n-1}$ is the average aquifer pressure in t_{n-1} ,MPa; $(\bar{p}_r)_n$ is the reservoir pressure in t_n ,MPa; J is influx index, $\text{m}^3/\text{day}/\text{MPa}$; W_{ei} is the maximum water influx, m^3 ; they can be calculated by the follow formula:

$$J = \frac{0.5358 k_a h f}{\mu_w \left[\ln(r_a/r_e) - 0.75 \right]} \tag{12}$$

$$(\bar{p}_a)_{n-1} = p_i \left(1 - \frac{(W_e)_{n-1}}{W_{ei}} \right) \tag{13}$$

$$(\bar{p}_r)_n = \frac{(p_r)_n + (p_r)_{n-1}}{2} \tag{14}$$

$$W_{ei} = \pi (r_a^2 - r_e^2) h \phi c_i p_i \left(\frac{\theta}{360^\circ} \right) \tag{15}$$

3 Application of material balance analysis

Based on the research of domestic and foreign scholars on material balance analysis, this paper proposes an idea and method that combines the classical material balance analysis method with reservoir numerical simulation technology: (1) global sensitivity parameters such as reserves and water parameters are obtained through material balance calculation, which play a decisive role in the overall dynamic characteristics of the reservoir, and can be used as the initial optimization parameter combination of reservoir numerical simulation (2) analyze the uncertainty of the parameters, reduce the adjustment range of some adjustable parameters in the history matching, and determine the reasonable adjustment range.

3.1 Global sensitivity parameter estimation

As for the calculation of reserves, some experts have proposed some effective methods since the middle of last century[7-9], the most widely used methods are Havlena-Odeh

method[10], Campbell method[11] and Tehrani method [12].

3.1.1 Havlena-Odeh method

Havlena and Odeh recombined the linear form of the material balance equation as follows:

$$\frac{F}{E_t} = N + \frac{W_e}{E_t} \tag{16}$$

If W_e can be expressed as:

$$W_e = US(p,t) \tag{17}$$

Then:

$$\frac{F}{E_t} = N + U \left(\frac{S}{E_t} \right) \tag{18}$$

where U is water influx constant, rm^3/day ; S is the water body function, and its expression is different for different types of water bodies [13].

If the water model is correct, $F/E_t - S/E_t$ should be a straight line with slope U and intercept N as shown in Figure 1. When using this method to determine the reserves and water influx constant, we need to use the trial and error method, and constantly assume different water body parameters until F/E_t and S/E_t meet the linear relationship.

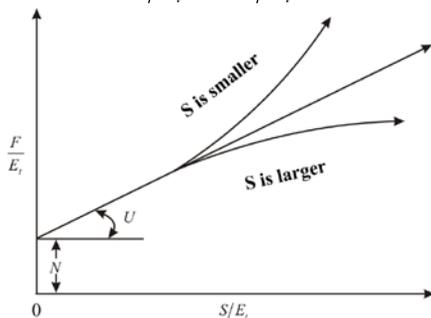


Fig. 1. Havlena-Odeh linear relationship.

3.1.2 Tehrani method

Tehrani pointed out that equation (18) is sensitive to the error of average pressure, and proposed that the least square regression should be directly applied to equation (1) to determine reserves and water influx constant [12].

The measured and calculated deviations of F is defined as follows:

$$z = NE_t + US - F \tag{19}$$

Then the sum of squares of errors is:

$$SSD = \sum_{i=1}^{i=n} z_i^2 \tag{20}$$

Reserve N and water influx constant U can be obtained by minimizing SSD . Similar to the Havlena-Odeh method, equation (19) needs to determine the water body function S first.

3.1.3 Campbell method

Campbell proposed a linear form of the material balance equation:

$$\frac{F - W_e}{E_t} = N \tag{21}$$

When there is no water influx, F/E_t with respect to F should be a horizontal line with the value of N ; when the amount of water influx increases, the calculated value of N increases continuously. When the line of F/E_t with respect to F is extended to $F = 0$, N can be obtained.

Generally, Campbell curve is used to judge the intensity of water influx, as shown in Fig. 2:

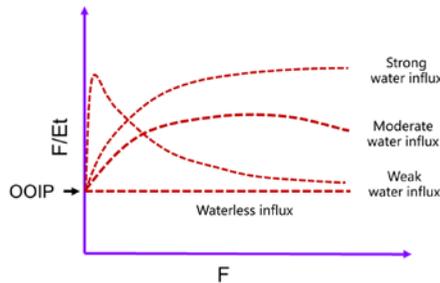


Fig. 2. Campbell theoretical curve.

3.1.4 The solution method used in this paper

There are many unknown parameters involved in the mass balance equation, especially the calculation of water influx. The traditional calculation method needs many times of manual calculation, so the calculation efficiency is low. In order to make the calculation results more accurate and reliable, this paper uses the method of combining nonlinear regression and linear regression to comprehensively determine the reserves and water body parameters. The technical route is shown in Fig. 3.

The process of nonlinear regression is: the square of the difference between the measured value and the calculated value of cumulative oil production is taken as the objective function, and the reserves and water body parameters can be obtained by calculating the minimum value of the objective function. Therefore, the problem is transformed into the following nonlinear regression problems:

$$c_{k+1} = \arg \min \{f(c)\} \tag{22}$$

$$f(c) = \frac{1}{2} \sum_{i=1}^{i=N} \left(\frac{N_{pcal,i} - N_{pobv,i}}{w_i} \right)^2 \tag{23}$$

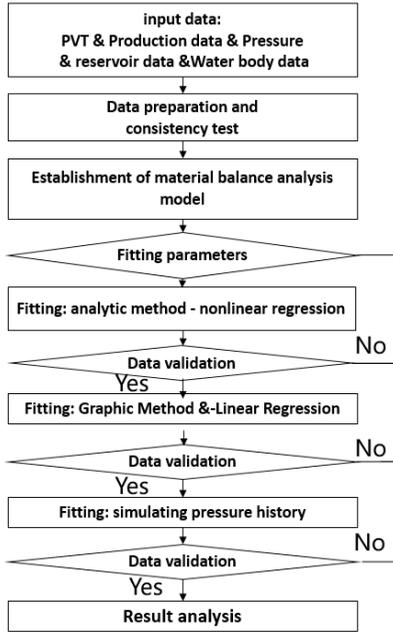


Fig. 3. Calculation process of global sensitivity parameters.

That is, solving a set of parameters c makes $f(c)$ minimum. The Levenberg-Marquardt method is used in the nonlinear regression program [14], and the iterative formula is shown in equations (24) and (25)

$$\left[J^T W J + \lambda \text{diag} \left(J^T W J \right) \right] h = J^T W D \tag{24}$$

$$c_{k+1} = c_k + h \tag{25}$$

Where J is Jacobian matrix, $J_{ij} = \frac{\partial N_{pcal,i}}{\partial c_i}$; W is weight matrix; λ is damping coefficient;

D is difference between calculated value and measured value.

For the linear regression method, since the calculation model of Fetkvoic quasi steady water body and Carter-Tracy unsteady water body can not be expressed as the form shown in equation (17), the Havlena-Odeh linear equation and the Tehrani method are no longer applicable. In this paper, equation (1) is written as follows:

$$F - W_e = N E_i \tag{26}$$

Then $F - W_e$ with respect to E_i should be a straight line with slope N and passing through the origin. According to this feature, the correctness of the water parameters obtained by the nonlinear regression method can be verified and the reserves N can be obtained.

3.2 Uncertainty analysis

Although reservoir numerical simulation has become a mature technology, there is still a problem that has not been solved well, that is, the uncertainty of the model. The parameters describing reservoir geology and fluid properties, as well as the recorded historical data of production performance, have varying degrees of uncertainty. In this paper, Monte-Carlo simulation method is used to analyze the uncertainty of numerical simulation model, which can recognize and reduce the uncertainty of numerical simulation model. The specific process can be divided into the following steps:

(1) The source and degree of uncertainty of basic data are analyzed.

(2) Set the uncertainty error range of basic data, and use random sampling method to generate N groups of basic data with a certain error range, they obey the random error of certain distribution, or have the deterministic error set manually

(3) Based on the material balance calculation, Monte-Carlo simulation is carried out. The uncertainty of the simulation prediction results is analyzed by using the statistical principle, and compared with the measured data, the adjustable range of the uncertain parameters in the numerical simulation is determined.

4 Example analysis

4.1 Theoretical calculation example

Based on the PUNQ-S3 model [15], a group of production data is built for material balance theoretical analysis by numerical simulation. The data is as Table 1. The model information is as follows. The grid of the three dimensional three phase black oil model is $19 \times 28 \times 5$, and there are two faults in the west and south side, and water body is connected in the west and north. There are 5 producers and no injector. Production history is 16.5 years including 1 year for test and 3 years for shut and production for 12.5 years. The reserve is calculated about $17.373 \times 10^6 \text{sm}^3$ by volumetric method. The reservoir and water parameters in the numerical simulation are list in table 2. The PUNQ-S3 model is used because the complexity of this theoretical model is fit for the realistic reservoir. The target of this example is to show the reasonability to get the global sensitivity parameters of numerical simulation using material balance method and verify the calculation result.

4.1.1 Reserve and water body calculation

Calculating the F and Et by the data in table 1, and Campbell curve is drawn, as Figure 4.

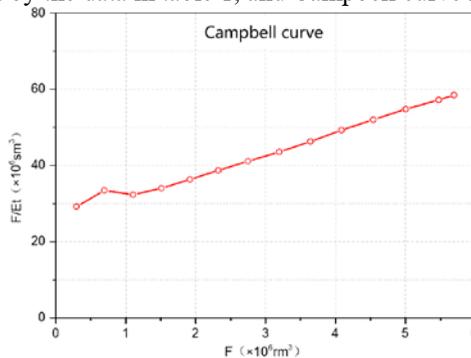


Fig. 4. Campbell curve of theoretical example.

Table 1. PUNQ-S3 reservoir production parameters.

| Date (yr.) | P (MPa) | Np (MMSm3) | Gp (MMSm3) | Wp (MMSm3) | Bo (m3/Sm3) | Rs (Sm3/Sm3) | Bg (m3/Sm3) | Bw (m3/Sm3) |
|------------|---------|------------|------------|------------|-------------|--------------|-------------|-------------|
| 0 | 23.446 | 0.000 | 0.000 | 0.000 | 1.2000 | 74.0000 | 0.0044 | 1.0238 |
| 1 | 22.978 | 0.246 | 17.749 | 0.000 | 1.1969 | 72.5004 | 0.0045 | 1.0240 |
| 2 | 22.978 | 0.246 | 17.749 | 0.000 | 1.1968 | 72.4975 | 0.0045 | 1.0240 |
| 3 | 22.977 | 0.246 | 17.749 | 0.000 | 1.1968 | 72.4963 | 0.0045 | 1.0240 |
| 4 | 22.977 | 0.246 | 17.749 | 0.000 | 1.1968 | 72.4956 | 0.0045 | 1.0240 |
| 5 | 22.501 | 0.574 | 42.143 | 0.000 | 1.1935 | 70.9642 | 0.0046 | 1.0243 |
| 6 | 21.919 | 0.891 | 70.851 | 0.000 | 1.1894 | 69.0895 | 0.0047 | 1.0246 |
| 7 | 21.500 | 1.207 | 97.829 | 0.000 | 1.1865 | 67.7397 | 0.0048 | 1.0248 |
| 8 | 21.164 | 1.523 | 123.720 | 0.002 | 1.1842 | 66.6571 | 0.0049 | 1.0250 |
| 9 | 20.879 | 1.839 | 149.072 | 0.010 | 1.1822 | 65.7409 | 0.0050 | 1.0252 |
| 10 | 20.619 | 2.156 | 174.076 | 0.032 | 1.1803 | 64.9083 | 0.0050 | 1.0253 |
| 11 | 20.375 | 2.459 | 198.691 | 0.086 | 1.1786 | 64.1244 | 0.0051 | 1.0255 |
| 12 | 20.182 | 2.739 | 222.790 | 0.161 | 1.1773 | 63.5042 | 0.0052 | 1.0256 |
| 13 | 20.024 | 3.008 | 245.975 | 0.249 | 1.1762 | 62.9958 | 0.0052 | 1.0257 |
| 14 | 19.876 | 3.267 | 268.310 | 0.357 | 1.1751 | 62.5198 | 0.0052 | 1.0257 |
| 15 | 19.737 | 3.515 | 289.742 | 0.485 | 1.1742 | 62.0725 | 0.0053 | 1.0258 |
| 16 | 19.589 | 3.758 | 310.640 | 0.627 | 1.1731 | 61.5966 | 0.0053 | 1.0259 |
| 16.5 | 19.533 | 3.873 | 320.369 | 0.697 | 1.1727 | 61.4172 | 0.0054 | 1.0259 |

Table 2. Reservoir and water body parameters.

| Reservoir parameters | | Water parameters | |
|---------------------------------|-----------------------|------------------------------|--------------------------|
| Initial pressure/MPa | 23.616 | thickness/m | 19.6 (west) ,6.0 (north) |
| Saturation pressure/MPa | 23.4 | Inside radius/m | 3000 |
| Water saturation | 0.365 | outside/inside radius | ∞ |
| Cr/MPa ⁻¹ | 4.50×10^{-5} | Waterinfluxangle/ $^{\circ}$ | 95 |
| Cw/MPa ⁻¹ | 5.43×10^{-6} | Permeability/mD | 137.5 |
| Oil reserve/ 10^6sm^3 | 17.373 | Porosity | 0.213 |
| Gas reserve/ 10^6sm^3 | 364.654 | Water body type | Carter-Tracy |

From the figure4 we can judge that strong water influx exists in the reservoir. So the water influx volume is needed to consider when the material balance is analyzed.

The reserve and the water body parameter are analyzed by linear regression and the result is as figure 5.

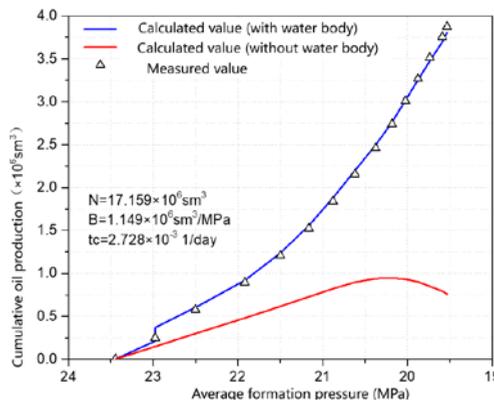


Fig. 5. Non-linear regression curve.

From figure 5 the result difference is obvious with water body and without water body. It shows that water influx affects the material balance calculation much. The calculated oil reserve is $17.159 \times 10^6 \text{sm}^3$, similar with the volume method result. The water influx constant B and time dimensionless factor t_c are calculated by the water body parameter from the regression analysis..

Based on the water parameter from the non-linear regression, the relationship curve about $F - W_e$ and E_t is drawn as figure 6. The linear relationship of $F - W_e$ and E_t is confirmed, and the reserve is calculated by the linear least squares analysis and the result is $17.365 \times 10^6 \text{sm}^3$, which is fit with the non-linear regression result.

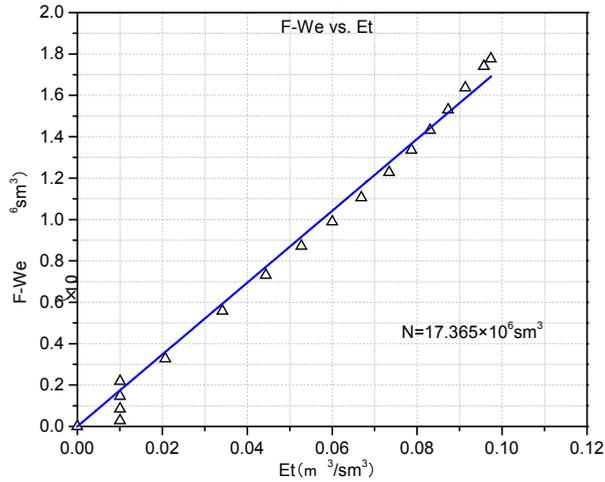


Fig. 6. Linear regression curve.

Finally the pressure is calculated by the parameters got from the regression analysis, and the test pressure is compared with the calculated data in figure 7. Two pressure is in consistent law of change, which shows the calculation result is correct.

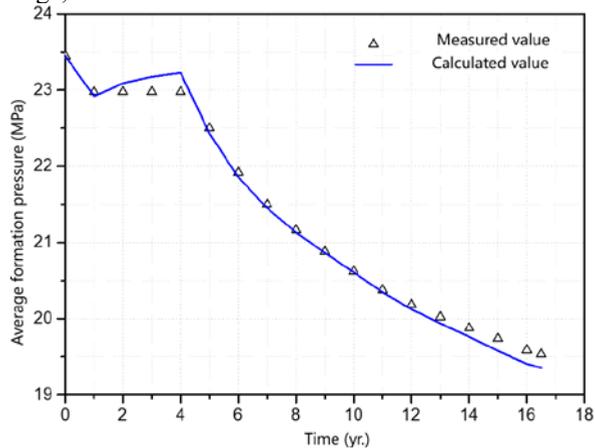


Fig. 7. Calculation pressure and test pressure comparison.

Now we finish the calculation of reserve and water body parameters as the process of figure 3, and next we will confirm the reasonability of the result.

4.1.2 Result confirm

From the above analysis we can see the reserve calculated is fit with the numerical simulation data. The water influx is calculated by water influx model and by numerical simulation in figure 8. The water influx volume calculated by material balance is similar with that got by simulation, which shows the material balance can obtain the input parameters for the numerical simulation.

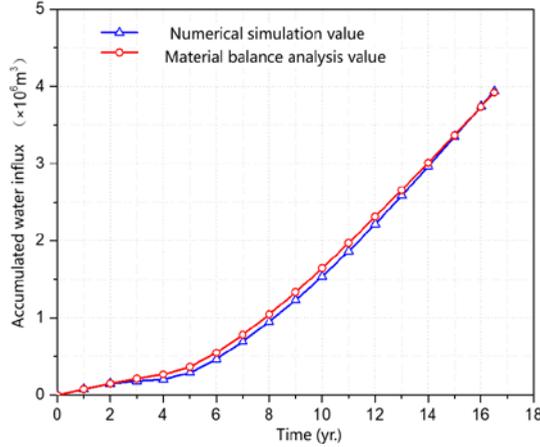


Fig. 8. Water influx calculated by two methods.

Two water bodies are set in the numerical simulation model. But only one set parameter is got in the material balance calculation. Though the parameters got from the material balance calculation cannot be one to one correspondence relationship with simulation model, the water influx volume is coincidence with the real reservoir. So the water influx volume can be the standard data put in the model and need not adjust often.

4.2 Real reservoir example

The real reservoir example is an oil field in the east area of china and developed form 1970. The oil field lies in the middle of the anticlinal structure of the fornix and there are 85 wells totally. The pressure and the water cut test data are list in figure 9 compared with the initially calculated data in the numerical model.

From the figure 9 we can see, the difference between the test data and the simulation data. And the pressure calculated increases fast and has great difference with the realistic production data. The last time set in the model is 11748 days and the numerical calculation stop at 6452 days due to the non-convergence. The reason of the difference is analyzed and the injection split is not correct and is big uncertain. The uncertainty analysis method is used to confirm the change of the range of injection volume. And then the injection volume is corrected.

The reservoir has no natural water by the geological research. So the material balance equation can be simplified to the follows.

$$F = NE_t \tag{27}$$

Then the material balance equation in t_1 time is as follows.

$$F_1 = NE_{t_1} \tag{28}$$

the material balance equation in t_2 time is as follows.

$$F_2 = NE_{i2} \tag{29}$$

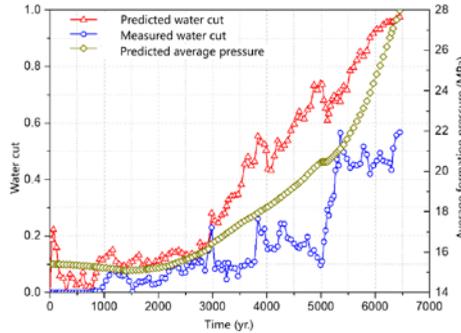


Fig. 9. The initial calculated result of simulation.

Suppose $t_2 > t_1$ and $\Delta t = t_2 - t_1 \approx 0$, and due to the reservoir pressure changes slowly, and we can think $p_1 = p_2$, and then $E_{i2} = E_{i1}$. From (26) and (25) divide Δt ,

$$q_o (B_o - B_g R_s) + (q_g - i_g) B_g + (q_w - i_w) B_w = 0 \tag{30}$$

The q_o , q_g , q_w , i_g and i_w is oil rate, gas rate, water rate and water injection rate, sm^3/day .

Changing the form and getting the water injection rate as follows.

$$i_w B_w = q_o (B_o - B_g R_s) + (q_g - i_g) B_g + q_w B_w \tag{31}$$

The injection volume can be calculated by equation (31) when the production, formation volume factor, R_s is obtained. It should be noted that equation (31) don't consider the natural water body, and not universal for other model. If the natural water influx is taken into consideration, then the calculated water injection rate i_w is the sum of the natural water influx and injection water. Almost all the oil field are put into production with water injection, and natural water influx is little proportion so the equation (31) can be used approximately.

Due to the measurement error the production, formation volume factor, R_s is uncertainty. In this example we are short of the whole pressure testing data. And the uncertainty is added. So we choose Monte-Carlo simulation method to predict the water injection.

First the data uncertainty is analyzed. Because the oil production is the most important data in the whole oil field management. The measurement and statistic is relatively correct. But the water and gas production data is not so accuracy. The measurement in separator has also big error except normal test and human factor. The production of dissolved gas is not measured and the uncertainty is so big. Due to the less of separate measuring, the injection data in different layer is uncertainty too. The error is increased by the measurement condition and the inaccurate correction. The error of pressure data comes from the tools calibration, frequency of measurement and fluid gradient. The PVT data of crude oil and natural gas come from the testing in the laboratory, and then the PVT data has big uncertainty due to the different condition between the laboratory and formation. Usually the oil field lacks the initial data of the earlier time and need to give the reasonable assumption.

Based on the above analysis and combined with the realistic condition, we assume the error of quantity, formation volume factor, R_s is normal distribution, and the standard

deviation of every parameter is q_o -5%, q_w -10%, q_g -20%, B_o -15%, B_g -20%, B_w -5%, R_s -15%. The simulation is done for 3000 times, and the average of water injection, P10, P50, P90 as figure 10.

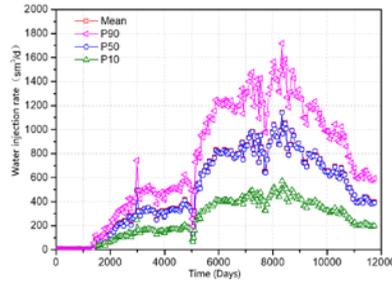


Fig. 10. The prediction of water injection.

The formation pressure change is predicted by simulation using the average, P10, P50, P90 injection data. And it is compared with the test data in figure 11. The predicted pressure changes in the range of the test pressure, and the calculated result is get better.

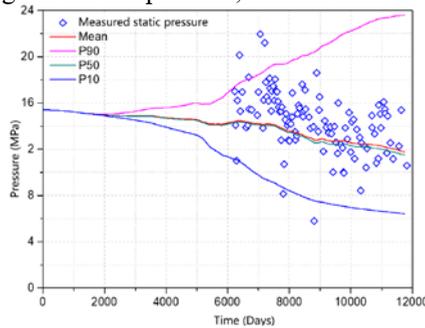


Fig. 11. The comparison of formation pressure.

Finally we use the calculated average injection data to do the numerical history matching, and the water cut matching curve in figure 12 is getting better and the precision of the simulation is increased by the correction injection data.

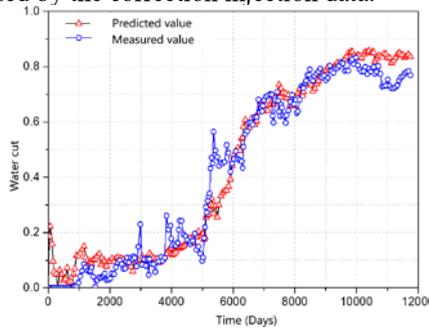


Fig. 12. The matching result of water cut.

5 Conclusion

(1) This paper presents a method of accelerating the history fitting of reservoir numerical simulation by material balance analysis optimization, and puts forward the specific

implementation scheme from the determination of global sensitivity parameters and uncertainty analysis.

(2) The established global sensitivity parameter solving method can obtain more accurate basic reservoir parameters, including reserves and water parameters, and provide better initial conditions for numerical simulation.

(3) The established uncertainty analysis method can analyze the influence of parameter uncertainty and determine the adjustable range of parameters.

(4) Material balance analysis is a very important work before the exquisite three-dimensional numerical simulation, which provides a macro overall understanding and reduces uncertainty.

References

1. Schilthuis R J. Active oil and reservoir energy [J]. Transactions of the AIME, 1936, 118(01): 33-52.
2. Dake L P. Fundamentals of reservoir engineering [M]. Elsevier, 1983.
3. Hurst W. Water influx into a reservoir and its application to the equation of volumetric balance [J]. Transactions of the AIME, 1943, 151(01): 57-72.
4. Van Everdingen A F, Hurst W. The application of the Laplace transformation to flow problems in reservoirs [J]. Journal of Petroleum Technology, 1949, 1(12): 305-324.
5. Carter R D, Tracy G W. An improved method for calculating water influx[J]. 1960.
6. Fetkovich M J. A simplified approach to water influx calculations-finite aquifer systems [J]. Journal of Petroleum Technology, 1971, 23(07): 814-828.
7. Stewart F M, Callaway F H, Gladfelter R E. Comparison of Methods for Analyzing a Water Drive Field, Torchlight Ten Sleep Reservoir, Wyoming[J]. Journal of Petroleum Technology, 1954, 6(09): 105-110.
8. Irby T L, Zurawsky L G, Clapham E E. Material-balance analysis of a water-drive reservoir with an unusual development history [J]. Journal of Petroleum Technology, 1962, 14(01): 37-42.
9. McEwen C R. Material balance calculations with water influx in the presence of uncertainty in pressures [J]. Society of Petroleum Engineers Journal, 1962, 2(02): 120-128.
10. Havlena D, Odeh A S. The material balance as an equation of a straight line [J]. Journal of Petroleum Technology, 1963, 15(08): 896-900.
11. Campbell J M, Campbell R A. Mineral property economics [M]. Campbell Petroleum Series, 1978.
12. Tehrani D H. An analysis of volumetric balance equation for calculation of oil-in-place and water influx [C]. Fall Meeting of the Society of Petroleum Engineers of AIME. Society of Petroleum Engineers, 1972.
13. Wang B, Litvak B L, Bowman G W. OILWAT-Microcomputer program for oil material balance with gas cap and water influx [J]. SPE Computer Applications, 1992, 4(05): 8-19.
14. Marquardt D W. An algorithm for least-squares estimation of nonlinear parameters [J]. Journal of the society for Industrial and Applied Mathematics, 1963, 11(2): 431-441.
15. Website, PUNQ, <http://www.nitg.tno.nl/punq/>.