

# Bioconvection of Nanofluid Past Stretching Sheet in a Porous Medium in Presence of Gyrotactic Microorganisms with Newtonian Heating

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**Abstract.** In this study, the effect of Newtonian heating on the boundary layer flow and heat transfer over a stretching surface in a porous medium in the presence of gyrotactic microorganisms and nanoparticle fractions are analysed. The governing equations are reduced to a system of couple non-linear ordinary differential equations, subjected to the Boussinesq approximation and asymmetric heat conditions. The reduced governing ordinary differential equations are then solved numerically. The solutions obtained are graphically represented. The effects of the controlling parameters on the flow, heat, nanoparticle concentration and the density of motile microorganisms have been examined. The results of the present study show the flow velocity, heat and mass transfer and motile microorganism characteristics on the stretching sheet are strongly influenced by the bioconvection parameters and Newtonian.

## 1 Introduction

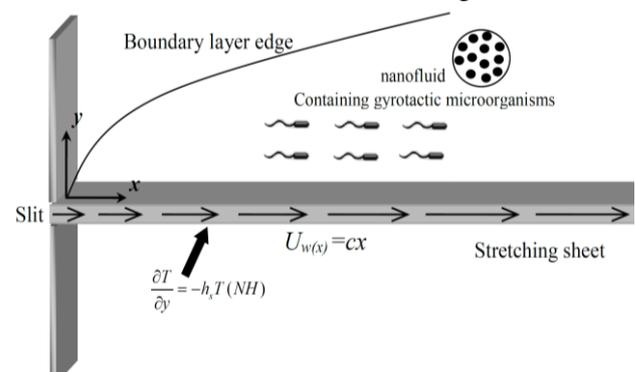
The concept of bioconvection and nanofluid in biological porous media which is the emphasis of current work has many applications in medical engineering and biotechnological systems [1, 2]. Nanofluid is considered as a fluid in which solid nanoparticles with the length scales of 1-100 nm are suspended in conventional heat transfer basic fluid. It has many practical applications in several engineering processes and medical sciences, such as heat pipes [3], biofuel cells [4] and biomimetic microsystems [5]. Many researchers have focused on modeling the thermal conductivity and examined different viscosities of nanofluids over the past decade. The addition of nanoparticles to base fluids to improve their thermal conductivity and enhance the heat transfer performance was first demonstrated by Choi [6]. Several experimental and numerical analyses about nanofluid heat transfer performance can be found in Refs. [7-14].

Recently, the Buongiorno's model [15], who considered seven slip mechanisms which can produce a relative velocity between the nanoparticles and the base fluid, was further developed by Kuznetsov [16] to study the influence of using motile microorganisms for enhancing mass transport, inducing mixing and prevent nanoparticle agglomeration in nanofluids. Bioconvection in nanofluids occurs if the concentration of nanoparticles is little so that nanoparticles do not cause any significant increase in the viscosity of the base fluid. Nield and Kuznetsov [17, 18] used the mathematical nanofluid model proposed by Buongiorno to study the boundary layer flow of nanofluid in a porous medium. To the best of authors' knowledge, there is not any investigation to

address the effect of the Newtonian heating boundary condition on the heat transfer characteristics of bioconvection of nanofluid flow over stretching sheet in a porous medium. The present study aims to examine the effect of the Newtonian heating boundary condition on the heat transfer characteristics of stretching sheet in the presence of nanoparticles and their dynamic effects.

## 2 Governing equations

Consider a two-dimensional incompressible and steady state viscous flow past a convectively heated vertical flat plate embedded in a porous medium filled with nanofluid containing gyrotactic microorganisms. It is assumed that there is no nanoparticle agglomeration, and the porous matrix does not absorb microorganisms and that the pore sizes are significantly larger than the microorganisms. Also, the presence of nanoparticles was assumed to have no effect on the direction in which microorganisms.



**Figure 1.** The physical sketch and coordinate system.

The velocity of the surface is linear and is taken as  $U_{w(x)} = c.x$  where  $c$  is a constant, and  $x$  is the coordinate component measured along the stretching surface. The physical model and coordinate system of this problem are shown in Figure 1.

We assume that the wall is subjected to a Newtonian heating boundary condition (NH). Using scale analysis and applying the boundary layer approximations, the governing equations can be written as [19]:

$$\rho_f \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \quad (1)$$

$$-\sigma B_0^2 u - \frac{\mu u}{\kappa} + g \left[ \begin{array}{l} (1-C_\infty)\rho_f \beta (T-T_\infty) \\ -(\rho_p - \rho_f)(C-C_\infty) \\ -(n-n_\infty)\lambda(\rho_{m\infty} - \rho_f) \end{array} \right]$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left( \frac{\partial^2 T}{\partial y^2} \right) + \tau \left\{ \begin{array}{l} D_B \left( \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} \right) + \\ \frac{D_T}{T_\infty} \left[ \left( \frac{\partial T}{\partial y} \right)^2 \right] \end{array} \right\} + \quad (2)$$

$$\frac{\mu \alpha}{k} \left( \frac{\partial u}{\partial y} \right)^2 + \frac{\alpha \sigma B_0^2 u^2}{k}$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_B \left( \frac{\partial^2 C}{\partial y^2} \right) + \left( \frac{D_T}{T_\infty} \right) \left( \frac{\partial^2 T}{\partial y^2} \right) \quad (3)$$

$$u \frac{\partial n}{\partial x} + v \frac{\partial n}{\partial y} + \frac{bW_c}{(C_w - C_\infty)} \left[ \frac{\partial}{\partial y} \left( n \frac{\partial C}{\partial y} \right) \right] = D_n \left( \frac{\partial^2 n}{\partial y^2} \right) \quad (4)$$

The corresponding boundary conditions are taken as:

$$\left\{ \begin{array}{l} v = 0, u = U_w(x) \\ -\frac{\partial T}{\partial y} = h_s(x)T, C = C_w, n = n_w \end{array} \right\} : at y = 0, \quad (5)$$

$$\left\{ \begin{array}{l} v \rightarrow 0, u \rightarrow 0, T \rightarrow T_\infty \\ C \rightarrow C_\infty, n \rightarrow n_\infty \end{array} \right\} : at y \rightarrow \infty$$

Where  $h_s$  is the heat transfer parameter. To attain similarity solution of equations (1)-(4), the stream function and dimensionless variables can be posited in the following form:

$$\psi = \alpha Ra_x^{1/4} f(\eta), \eta = \frac{y}{x} Ra_x^{1/4}, \theta(\eta) = \frac{T - T_\infty}{T_\infty} \quad (6)$$

$$Ra_x = \frac{(1-C_\infty)\beta g \rho_f T_\infty x^3}{\alpha \nu}, \beta(\eta) = \frac{C - C_\infty}{C_w - C_\infty}, \phi(\eta) = \frac{n - n_\infty}{n_w - n_\infty} \quad (7)$$

By applying the similarity transforms on equations (1)-(4), the similarity equations are obtained as follows:

$$f''' + \frac{3}{4Pr} f f'' - Mf' + \theta - Nr\beta - Rb\phi - Af' = 0 \quad (8)$$

$$\theta'' + \frac{3}{4} f \theta' + Nb \beta' \theta' + Nt \theta'^2 + Ec Pr (f''^2 + Mf'^2) = 0 \quad (9)$$

$$\beta'' + \frac{Nt}{Nb} \theta'' + \frac{3}{4} Le f \beta' = 0 \quad (10)$$

$$\phi'' + \frac{3}{4} Lbf \phi' - Pe [\beta' \phi' + \beta''(\sigma + \phi)] = 0 \quad (11)$$

Subject to the dimensionless boundary conditions:

$$At \eta = 0 : \left\{ \begin{array}{l} f = 0, f' = 1, \\ \theta' = -\gamma(1 + \theta), \beta = 1, \phi = 1 \end{array} \right\} \quad (12)$$

$$At \eta \rightarrow \infty : f' = 0, \theta = 0, \beta = 0, \phi = 0$$

Where primes denote differentiation with respect to  $\eta$ . The parameters of the equation (8)-(11) are defined by:

$$Pe = \frac{bW_c}{D_n}, Le = \frac{\alpha}{D_B}, Lb = \frac{\alpha}{D_n}, A = \frac{x^2}{\kappa Ra_x^{1/2}}$$

$$Nb = \frac{(\rho c)_p D_B (\phi_w - \phi_\infty)}{(\rho c)_f \alpha}, Nt = \frac{(\rho c)_p D_T}{(\rho c)_f \alpha} \quad (13)$$

$$\sigma = \frac{n_\infty}{n_w - n_\infty}, M = \frac{\sigma B_0^2 x^2}{\nu \rho_f Ra_x^{1/2}}, Ec = \frac{\alpha^2 Ra_x}{x^2 C_p T_\infty}$$

$$Rb = \frac{\gamma(n_w - n_\infty)\Delta\rho}{\rho_f \beta(1 - C_\infty)T_\infty}, Nr = \frac{(\rho_p - \rho_f)\Delta C_w}{\rho_f \beta(1 - C_\infty)T_\infty}$$

Where Pr is the Prandtl number, Le is the traditional Lewis number, Pe is the bioconvection Peclet number, M is the modified magnetic parameter, Ec is the modified Eckert number, Nr is the buoyancy ratio parameter, A is the permeability parameter, Rb is the bioconvection Rayleigh number, Lb is the bioconvection Lewis number,  $\sigma$  is the bioconvection constant, Nb is the Brownian motion parameter and Nt is the thermophoresis parameter.

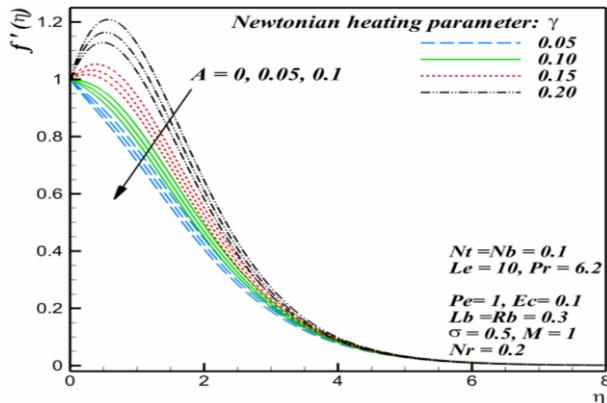
### 3 Results and discussion

The equations (8)–(11) subject to the boundary conditions (12) have been solved numerically for various range of Newtonian heating boundary condition and for different values of the permeability parameter, Prandtl number, the Lewis number, the buoyancy ratio parameter, the bioconvection constant and bioconvection Rayleigh number. Highly non-linear momentum boundary layer equation and thermal boundary layer equation are converted into similarity equations and then solved numerically by employing fifth order Runge-Kutta-Fehlberg scheme with shooting method [20].

The most crucial factor of this numerical solution is to choose the appropriate finite value of  $\eta_\infty$ . Thus, the asymptotic boundary conditions given by (15) were replaced by a comparatively large value  $\eta_{max}=15$  for the similarity variable ( $\eta_{max}$ ). The choice of  $\eta_{max}=15$  ensured that all numerical solutions approached to the asymptotic values correctly. It is worth mentioning to consider that the selection of a large value for  $\eta_{max}$  is an important point that is often overlooked in publications on the boundary layer flows. The details of the solution method can be found in [21].

Figure 2 shows the effect of permeability parameter and Newtonian heating parameter on the velocity field in the presence of bioconvection and nanofluid parameters. This figure illustrates that for increased the value of permeability parameter is to decrease the velocity distribution and consequently reduces the thickness of hydrodynamic boundary layer. This happens because of the presence of a porous medium that causes higher

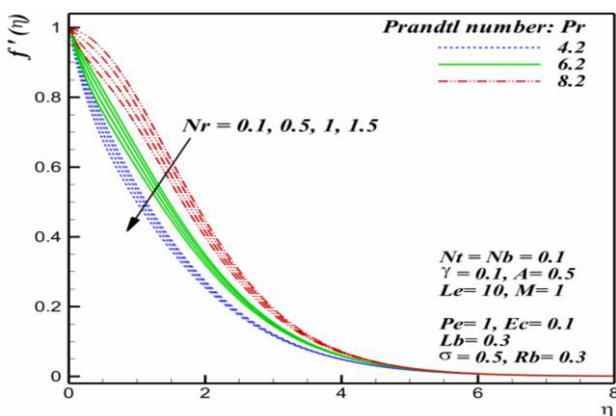
darcian drag force acting on the nanofluid and induce a deceleration in the flow. Furthermore, it is observed that dimensionless velocity rises in the boundary layer with increasing of the Newtonian heating parameter. This occurs due to the Newtonian heating decreases the density of nanofluid and as a result, the dimensionless velocity increases within the boundary layer.



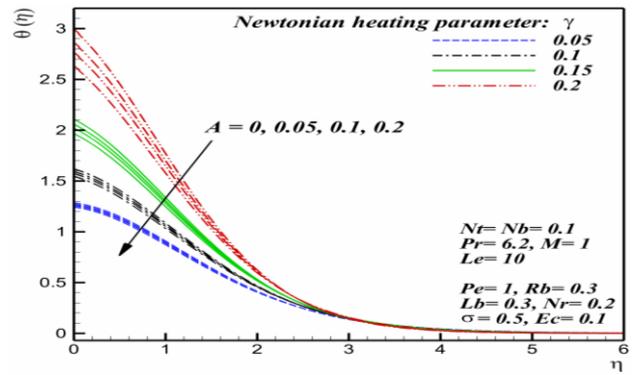
**Figure 2.** Effects of different parameters on dimensionless velocity

The influence of the buoyancy ratio parameter and Prandtl number on the velocity distribution of bioconvection nanofluid for a stretching sheet is presented in Figure 3. It is found that the dimensionless velocity increases with Prandtl number. The profile of dimensionless temperature for various values of parameter A and  $\gamma$  is shown in Figure 4.

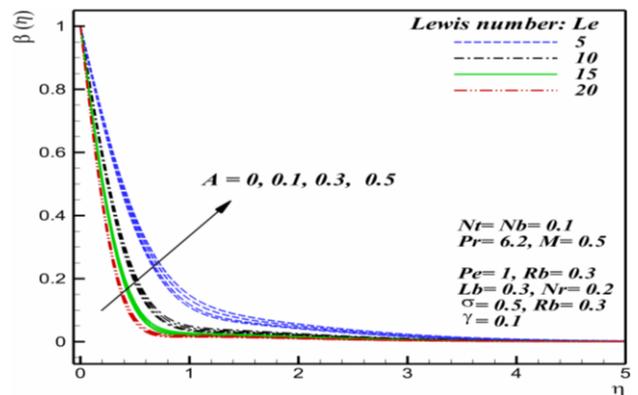
Figure 5 depict the influence of the permeability parameter and Lewis number on the dimensionless concentration. Figure 5 shows that the increase in the values of permeability parameter results in the increase in the concentration distribution in the boundary layer region. Also, nanoparticle volume fraction distributions decelerate with the increasing values of the Lewis number in the entire boundary layer region. The Lewis number represents the ratio of the thermal diffusivity to the mass diffusivity. Increasing the Lewis number means a higher thermal diffusivity and a lower mass diffusivity, and this produces thinner concentration boundary layer.



**Figure 3.** Effects of different parameters on dimensionless velocity.

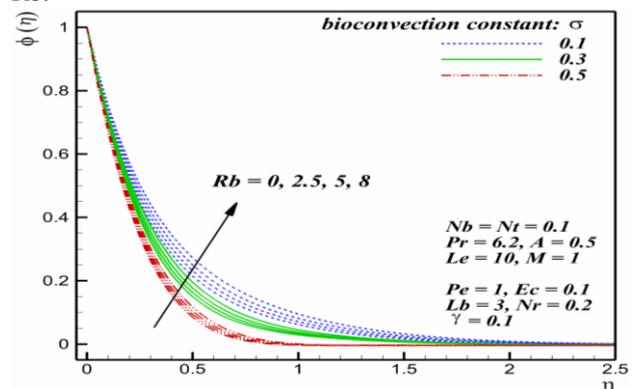


**Figure 4.** Effects of different parameters on dimensionless temperature

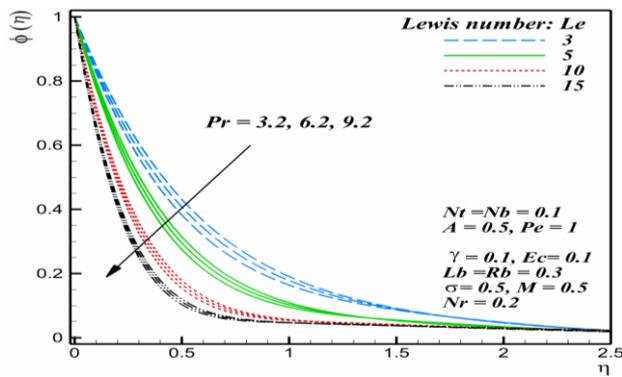


**Figure 5.** Effects of different parameters on dimensionless concentration.

The effect of bioconvection Rayleigh numbers and Lewis number on the rescaled density of motile microorganisms are shown in Figures 6 and 7. The variation of rescaled density of motile microorganisms respect to bioconvection Rayleigh number for different values of bioconvection constant are plotted in Figure 6. It can be seen that the density of motile microorganisms profile is relatively sensitive and strongly influenced by the changes in Rb and  $\sigma$  parameters. These graphs reveal that an increase in  $\sigma$  decreases the concentration thickness for the dimensionless density of motile microorganisms as well as the density of motile microorganisms. On the other hand, the dimensionless density of motile microorganisms increases with increase Rb.



**Figure 6.** Effects of different parameters on rescaled density of motile microorganisms.



**Figure 7.** Effects of different parameters on rescaled density of motile microorganisms.

## 4 Conclusions

MHD laminar boundary layer flow with heat and mass transfer on the bioconvection of electrically conducting incompressible nanofluid containing gyrotactic microorganisms past a vertical stretching sheet in a porous medium with Newtonian heating boundary condition are investigated numerically. Based on the results, the significant findings are as follows:

- Dimensionless velocity decreases with Permeability parameter and Buoyancy ratio parameter whereas it increases with Newtonian heating parameter and Prandtl number
- The increase of the Permeability parameter and Lewis number tends to decrease temperature and concentration. But the concentration and temperature increase with increasing Permeability parameter and Newtonian heating parameter.
- The rescaled density of motile microorganisms decreases with Lewis number, Prandtl number and bioconvection constant ( $\sigma$ ) and increase with increasing bioconvection Rayleigh numbers should be centred and should be numbered with the number on the right-hand side.

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