

above equation is a forward-finite-difference, which will be acquired under the liquid composition ($x_{i,j+1}$) as a function of $\Delta\xi$ (dimensionless time), which is obtained as follows (Henley *et al.*, 1998):

$$x_{i,j+1} = x_{i,j} + (y_{i,j} - x_{i,j}) \Delta\xi \tag{4}$$

Where the composition of the initial liquid in the bottom ($x_{i,j}$) and $\Delta\xi$ were determined, while the vapor composition ($y_{i,j}$) is calculated using the equation bubble T (Henley *et al.*, 1998).

Predecessor researchers for bioethanol made from starch have obtained quite good cellulose and bioethanol results. The purpose of this study was to look for alternative raw materials, reviewing the process of hydrolysis, fermentation, and batch distillation process to produce bioethanol with high ethanol content. In this research, we located raw materials from wastewater, using three processes (hydrolysis, fermentation and distillation batch) simultaneously and attained bioethanol production levels of 95-96% ethanol as substitute materials.

METHODOLOGY

From the results of laboratory analysis, it is known that ethanol-forming elements are glucose and starch. The average concentration of glucose is about 6%, starch in the rice is about 79%, while the starch in the rice flour wastewater is quite high, about 30%.

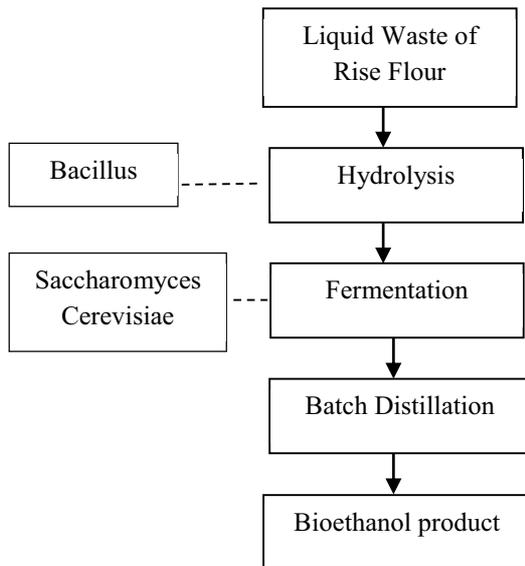


Figure-1. Chronology of bioethanol production using hydrolysis, fermentation and distillation batch

Pre-treatment was performed using waste water and filtration of plant rice flour to get a high glucose and starch and the hydrolysis process with the bacillus. A good quality bioethanol product is determined from several parameters, such as the degree of acidity (pH), Bacillus ratio for rice flour mill effluent, SC starter concentration, time of fermentation, and batch distillation time.

Quality analysis for raw materials and products of bioethanol was performed through laboratory work. The analysis was carried out by instrumentation and gravimetry, using Gas Chromatography (GC) and

Spectrophotometer, which analyzed the concentration of starch, glucose, ethanol, crude protein and N, P, K, Ca, Mg, S.

Hydrolysis process procedure

Hydrolysis process at figure 1 was performed under the following conditions: a temperature of 30 °C, hydrolysis time of 1 hour with 200 rotations per minute (rpm). The varied conditions were: the ratios of the volume of liquid waste bacillus were 1:2; 5:4; 10:7 and volume of: 5, 7, 9, 11, and 13 (% v/v). Once the process is completed, we obtained filtrate and solids. The filtrate would be processed using fermentation to obtain ethanol and solids levels can then be used as composts.

Fermentation process procedure

The result of glucose hydrolysis process has not qualified yet, so the next step is adding citric acid or NaOH. Citric acid is added to the filtrate until it reached a fermentation pH of 4.5, approximately. Next is adding the starter to the fermented solution in an anaerobic condition. In the fermentation process (Figure 1), the permanent conditions were a temperature of 30 °C, pH of 4.5; and the fermentation volume is equal to the amount of filtrate volume of hydrolysis process results. The changed conditions were varying the ratios of the volume of Bacillus waste which were: 1:2; 5:4; and 10:7 with the addition of Saccharomyces cereviceae of: 5, 7, 9, 11, and 13 (% v / v) and fermentation time of 4, 6, 8, 10, and 12 days, then continued with performing ethanol level analysis.

Distillation process procedure

Results obtained from the fermentation were inserted into the distillation flasks to obtain ethanol from glucose. Batch distillation process as shown in Figure 1 was run at a temperature of 78°C, equipped with a total condenser and heater. After the volume of the solution reached 10% of the volume of bottom feed, the batch distillation was stopped, and then the solution was analyzed for its level of ethanol.

RESULTS AND DISCUSSION

Quality Raw Materials

Liquid waste used as study materials was derived from rice flour waste from PT. Boga Sari mill. Carbohydrates are the main source of calories for humans, apart from protein and fat. Carbohydrates having the chemical formula of (CH₂O)_n, are formed from the reaction of CO₂ and H₂O with the help of sunlight through the process of photosynthesis in plant cells that contain chlorophyll. Ingredients that are a source of carbohydrates come from roots and stems of plants such as cassava, sago, and sugar cane; whereas from grains are rice, corn and soybeans. Rice flour mill effluent is the raw material came from carbohydrates types of grains, such as rice.

According to the results of laboratory analysis, starch content in rice flour mill effluent is of 9.282%, averagely. This means that if all elements are completely hydrolyzed, a large amount of glucose will be obtained. From 100 liters of liquid waste of rice flour mill, we can produce a maximum of 9.282 liters of glucose. In addition to starch, glucose is also present in the flour wastewater,

increased in bulk. In 100 grams of flour liquid waste, glucose can be produced to a maximum of 3,786 liters. Noting the high composition of glucose and starch in the flour mill waste water, the hydrolysis process is expected to run perfectly, so that the amount of glucose and starch was actually relegated to 12.568 liter glucose. The process of filtering waste flour mill is done by using gauze and was done repeatedly to get a clean result before going to hydrolysis process. In addition to the natural filtration, sedimentation was also done by keeping it for a while so it would form naturally, and then the filtrate was taken and sedimentation were used as compost sediment.

The effect of pH on adding H-Cl can be determined. With additional volume greater than the H-Cl, a low pH would be obtained. Due to the required pH of the fermentation is 4.5, the addition of H-Cl volume by 7% v / v is the closest, for various volume of wastewater. Before performing the process of hydrolysis, the pH of the filtrate was measured in accordance with the provisions of the fermentation process which is approximately 4.5. To obtain a pH of 4.5, Na-OH was added if the pH of the filtrate was below 4.5, while citric acid was added if the pH of the filtrate was above 4.5.

Hydrolysis Process

Starch is a component that is more complex disaccharide; since starch must be broken using amylase into disaccharide components, such as maltose. By using enzyme or bacillus, maltose is hydrolyzed into glucose.

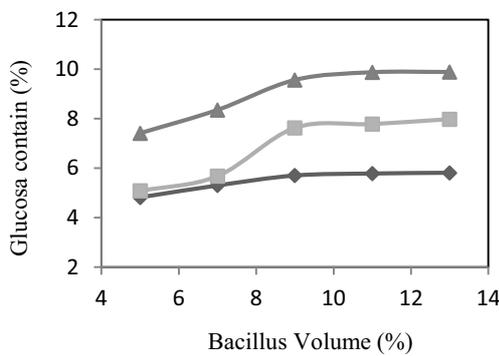


Figure-2. Changes on glucose contains with an addition of bacillus in liquid waste of rice flour (ratio bacillus/volume waste = 1:2: ♦, ratio bacillus /volume waste = 5:4: ■, ratio bacillus/volume waste = 10:7: ▲)

Figure 2 shows the effect of glucose levels for bacillus volume addition. The greater the volume of bacillus, the higher the level of glucose. On the addition of Bacillus volume above 9%, the graph shows a constant profile, because the performance of Bacillus began to decline and die from time to time, so it would be needed to add more Bacillus. The addition of Bacillus volume between (3-9) % v/v showed an increase in glucose levels, therefore showing the growth phase of Bacillus, so it can decompose starch into glucose optimally. Before the fermentation process is done, the filtrate optimum glucose level was measured at about 16%; if the glucose level is more than 16%, dilution is done. If the glucose level is less than 16%, the addition of glucose is made.

Fermentation Process

The fermentation process is a fermentation process that does not use oxygen (anaerobic process). To control the production of ethanol from sugar is quite complex. Substrate concentration, oxygen, and ethanol products, all of them affect yeast metabolism, cell survival, cell growth, cell division, and the production of ethanol. Appropriate selection of yeast strains and a high tolerance for concentration substrate or alcohol is important to improve results. The first fermentation is basic maintenance of seeds fermentation or starter preparation. Starter was inoculated until it was ready to be a fermenter, and then put into the fermentation substrate, which used SC seed fermentation.

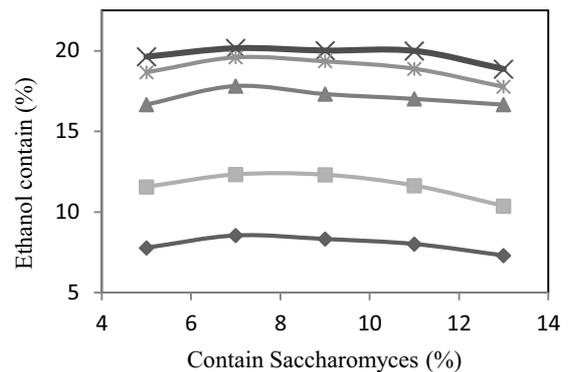


Figure-3. Changes on ethanol contains with an addition of Saccharomyces in liquid waste of rice flour (fermentation time = 4 days: ♦, fermentation time = 6 days: ■, fermentation time = 8 days: ▲, fermentation time = 10 days: x, fermentation time = 12 days: *)

Figure 3 shows the level of concentration of the filtrate which affects glucose residue. For a number of 6, 9, 11 and 13% v/v SC starters, the maximum residual glucose levels will be obtained in (1.3 - 3). The percentage, as in the reactor tank, of filtrate amount and SC starter were low hydrolyzed, so that the fermentation process is not optimal. By increasing the number of hydrolysis filtrate and SC beginner, residual glucose became smaller, because it has been fermented into ethanol.

After analyzing the residual glucose concentration of the fermentation process, the percentage of SC of the liquid (filtrate) was examined. In addition of 7%, it showed a smaller residual glucose levels compared to the addition of 6, 9, 11 and 13% starter. In initial research and Journal, an addition of 7% of the volume of fluid was admitted. The influence of the level of residual filtrate glucose levels, for 6, 9, 11 and 13% SC starters, a maximum residual glucose level was obtained in (1.5 to 5)%. It is because in the reactor tank, the filtrate is hydrolyzed and the SC starter is still low, so the fermentation process is not optimal. With the increasing number of hydrolyzed filtrate and SC starter, the residual glucose becomes smaller, since it was fermented into ethanol. According to preliminary research and the Journal, the best fermentation time is six days. Six days of fermentation is the best because it is the optimum phase of the SC. Below six days, there will be an adjustment to SC

growth and after six days there will be a regeneration phase or change phase of SC.

Batch Distillation Process

Ethanol is obtained from the fermentation and distillation batch process of mini-scale plant. By choosing the best

condition of fermentation, the fermentation time is 10 days. The concentration of ethanol from distillation batch shows the range of 95% to 96% and yield 31.66% to 33.3%. Economically, it meets the necessary technical requirements of ethanol, which is 95%, and the resulting yield is also high.

Table-1. Ethanol contain and yield on distillation batch

RatioHCl to raw materials	SC contain [%v/v]	Glucose contain [%v/v]	Ethanol contain [%v/v]	Ethanol contain [%v/v]	Yield [%]
1 : 2	5	4.82	19.63	91.5	30.5
	7	5.30	20.15	93	31,8
	9	5.70	20.01	94	32.3
	11	5.78	19.99	92.5	31.6
	13	5.81	18.87	91	32.3
5 : 4	5	5.08	18.63	92	30.2
	7	5.68	20.46	94.5	31.8
	9	7.63	20.88	96	33.3
	11	7.78	19.33	95	32.6
	13	7.98	18.27	94	32.1
10 : 7	5	7.41	19.63	94	30.4
	7	8.35	21.9	94.5	32.8
	9	9.56	20.44	95	33.1
	11	9.87	19.66	94.5	32.9
	13	9.88	18.77	93	32.6

CONCLUSIONS

Glucose levels of 9.98% were obtained in the process of hydrolysis of rice flour liquid waste, while ethanol in the fermentation process is 16% to 20.88%. Raw materials used to produce bioethanol indicate that the levels of ethanol 95% to 96% with ethanol yield 31.69% to 33.3% can be used to design a batch distillation column. By identifying the concentration and yield of ethanol, the liquid waste of rice flour raw material is more profitable than other raw materials.

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REFERENCES

Alok Kumar Dubey, P.K. Gupta, Neelam Garg, Sanjay Naithani. 2012. Bioethanol Production from Waste Paper Acid Pretreated Hydrolyzate with Xylose Fermenting *Pichia Stipitidis*. *Carbohydrate Polymers*, 88: 825-829.

Balat M, Balat H, Cahide O. 2008. Progress in Bioethanol Processing. *Progres Energy Combust Sci*, 34: 551-73.

Demirbas A. 2011. Competitive Liquid Biofuels from Biomass. *Applied Energy*, 88: 17-28.

Karimi K. Kheradmandinia S, Taherzadeh MJ. 2006. Conversion of Rice Straw to Sugars by Dilute Acid Hydrolysis. *Biomass and Bioenergy*, 30: 247 – 253.

Kuhad, R. C., Gupta, R., Khasa, Y. P., & Singh, A. 2010. Bioethanol Production from Lantana Camara (Red Sage) Pretreatment, Saccharification and Fermentation. *Bioresource Technology*, 101: 8348-8354.

Kumar, A., Singh, L., K., & Ghose, S. 2009. Bioconversion of Lignocellulosic Fraction of Water-Hyacinth (*Eichhornia Crassipes*) Hemicellulose Acid Hydrolysate to Ethanol by *Pichia Stipitidis*. *Bioresource Technology*, 100: 3293-3297.

Limayem A. Ricke SC. 2012. Lignocellulosic Biomass for Bioethanol Production; Current Perspectives, Potential Issues and Future Prospects. *Progres Energy Combust Sci*, 38: 449-67.

Nibedita Sarkar, Sumanta Kumar Ghosh, Satarupa Bannerjee, Kaustav Aikat. 2012. Bioethanol Production from Agricultural Wastes: An Overview. *Renewable Energy*, 37: 19-27.

Teymouri, F., Laureano-Peres, L., Alizadeh, H., & Dale, B, E. 2005. Optimization of the Ammonia Fiber Explosion (AFEX) Treatment Parameters for Enzymatic Hydrolysis of Corn Stover. *Bioresource Technology*, 96: 2014-2018.

Saravana Kannan Thangavelu, Abu Saleh Ahmed, Farid Nasir Ani. 2014. Bioethanol Production from Sago Pith Waste Using Microwave Hydrothermal Hydrolysis Accelerated by Carbon Dioxide. *Applied Energy*, 128: 277-283.